

Thermodynamics Relations

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Mathematical Theorems

- If there exists a relation among x , y & z ; $\rightarrow f(x, y, z) = 0$

$$\left(\frac{\partial x}{\partial y}\right)_z \left(\frac{\partial y}{\partial z}\right)_x \left(\frac{\partial z}{\partial x}\right)_y = -1$$

$$\left(\frac{\partial y}{\partial x}\right)_z \left(\frac{\partial x}{\partial y}\right)_z = \left(\frac{\partial y}{\partial z}\right)_x \left(\frac{\partial z}{\partial y}\right)_x = \left(\frac{\partial z}{\partial x}\right)_y \left(\frac{\partial x}{\partial z}\right)_y = 1$$

- $f(x, y, z) = 0 \rightarrow z = z(x, y)$, $y = y(z, x)$, $x = x(y, z)$

$$z = z(x, y) \rightarrow dz = \left(\frac{\partial z}{\partial x}\right)_y dx + \left(\frac{\partial z}{\partial y}\right)_x dy = Mdx + Ndy$$

For continuous functions, $\frac{\partial^2 z}{\partial x \partial y} = \frac{\partial^2 z}{\partial y \partial x} \Rightarrow \left(\frac{\partial M}{\partial y}\right)_x = \left(\frac{\partial N}{\partial x}\right)_y$



Maxwell's Relationships

- Internal Energy, $du = \delta q + \delta w = Tds - Pd v$ (for rev. process)
- Enthalpy, $h \equiv u + Pv \Rightarrow dh = du + Pd v + v dP = Tds + v dP$
- Helmholtz Energy, $f \equiv u - Ts \Rightarrow df = -Pd v - s dT$
- Gibbs Energy, $g \equiv h - Ts \Rightarrow dg = h dT - s dT + v dP - s dT = v dP - s dT$

For continuous functions, $\frac{\partial^2 z}{\partial x \partial y} = \frac{\partial^2 z}{\partial y \partial x} \Rightarrow \left(\frac{\partial M}{\partial y}\right)_x = \left(\frac{\partial N}{\partial x}\right)_y$

① $du = +Tds - Pd v \Rightarrow \left(\frac{\partial T}{\partial v}\right)_s = -\left(\frac{\partial P}{\partial s}\right)_v \dots\dots\dots (M01)$

② $dh = +Tds + v dP \Rightarrow \left(\frac{\partial T}{\partial P}\right)_s = +\left(\frac{\partial v}{\partial s}\right)_P \dots\dots\dots (M02)$

③ $df = -s dT - Pd v \Rightarrow \left(\frac{\partial s}{\partial v}\right)_T = +\left(\frac{\partial P}{\partial T}\right)_v \dots\dots\dots (M03)$

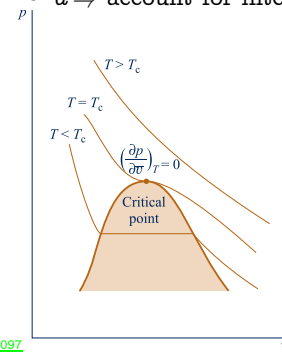
④ $dg = -s dT + v dP \Rightarrow \left(\frac{\partial s}{\partial P}\right)_T = -\left(\frac{\partial v}{\partial T}\right)_P \dots\dots\dots (M04)$



van der Waals' Equation

$$P = \frac{RT}{v-b} - \frac{a}{v^2}$$

- $b \Rightarrow$ account for the volume occupied by gas molecules
- $a \Rightarrow$ account for intermolecular forces of attraction.



At critical point: $\left(\frac{\partial P}{\partial v}\right)_T = \left(\frac{\partial^2 P}{\partial v^2}\right)_T = 0$
 $\Rightarrow v_c = 3b$, $a = \frac{27}{64} \frac{R^2 T_c^2}{P_c}$, $b = \frac{RT_c}{8P_c}$
 $\Rightarrow Z_c = \frac{P_c v_c}{RT_c} = \frac{3}{8} = 0.375$



C_v & Thermodynamics Relationships

- $du = Tds - Pd v \Rightarrow \left(\frac{\partial u}{\partial s}\right)_v = T$
- $C_v \equiv \left(\frac{\partial u}{\partial T}\right)_v = \left(\frac{\partial u}{\partial s}\right)_v \left(\frac{\partial s}{\partial T}\right)_v = T \left(\frac{\partial s}{\partial T}\right)_v$
- $\left(\frac{\partial C_v}{\partial v}\right)_T = \frac{\partial}{\partial v} \left[T \left(\frac{\partial s}{\partial T}\right)_v \right] = T \frac{\partial^2 s}{\partial v \partial T} = T \frac{\partial}{\partial T} \left[\frac{\partial s}{\partial v} \right]_T = T \left(\frac{\partial^2 P}{\partial T^2}\right)_v$
using Maxwell's relation: $\left(\frac{\partial s}{\partial v}\right)_T = + \left(\frac{\partial P}{\partial T}\right)_v$

If P-v-T data or mathematical relationship is available, it is possible to evaluate $\partial^2 P / \partial T^2$, and then $(\partial C_v / \partial v)_T$.

- Ideal gas: $Pv = RT$
 $\Rightarrow \left(\frac{\partial P}{\partial T}\right)_v = \frac{R}{v}, \left(\frac{\partial C_v}{\partial v}\right)_T = T \left(\frac{\partial^2 P}{\partial T^2}\right)_v = 0 \mapsto C_v \neq f(v)$
- van der Wall's gas: $P = \frac{RT}{v-b} - \frac{a}{v^2}$
 $\Rightarrow \left(\frac{\partial P}{\partial T}\right)_v = \frac{R}{v-b}, \left(\frac{\partial C_v}{\partial v}\right)_T = T \left(\frac{\partial^2 P}{\partial T^2}\right)_v = 0 \mapsto C_v \neq f(v)$



C_P & Thermodynamics Relationships

- $dh = Tds + v dP \Rightarrow \left(\frac{\partial h}{\partial s}\right)_P = T$
- $C_P = \left(\frac{\partial h}{\partial T}\right)_P = \left(\frac{\partial h}{\partial s}\right)_P \left(\frac{\partial s}{\partial T}\right)_P = T \left(\frac{\partial s}{\partial T}\right)_P$
- $\left(\frac{\partial C_P}{\partial P}\right)_T = \frac{\partial}{\partial P} \left[T \left(\frac{\partial s}{\partial T}\right)_P \right] = T \frac{\partial}{\partial T} \left[\frac{\partial s}{\partial P} \right]_T = -T \left(\frac{\partial^2 v}{\partial T^2}\right)_P$
using Maxwell's relation: $\left(\frac{\partial s}{\partial P}\right)_T = - \left(\frac{\partial v}{\partial T}\right)_P$
- Ideal gas: $\Rightarrow \left(\frac{\partial v}{\partial T}\right)_P = \frac{R}{P}, \left(\frac{\partial^2 v}{\partial T^2}\right)_P = 0 \mapsto C_P \neq f(P)$
- van der Wall's gas: $\Rightarrow \left(\frac{\partial v}{\partial T}\right)_P = \frac{R}{P - \frac{a}{v^2} (1 - \frac{2b}{v})}$
 $\left(\frac{\partial^2 v}{\partial T^2}\right)_P = - \frac{R^2 \left(\frac{2a}{v^3} - \frac{6ab}{v^4}\right)}{\left(P - \frac{a}{v^2} (1 - \frac{2b}{v})\right)^3} \mapsto C_P = f(P)$



Tds Relationships

- $s = s(v, T) \rightarrow ds = \left(\frac{\partial s}{\partial T}\right)_v dT + \left(\frac{\partial s}{\partial v}\right)_T dv$
 $C_v = T \left(\frac{\partial s}{\partial T}\right)_v$ & $\left(\frac{\partial s}{\partial v}\right)_T = + \left(\frac{\partial P}{\partial T}\right)_v$, Maxwell's Relation (C)
 $Tds = C_v dT + T \left(\frac{\partial P}{\partial T}\right)_v dv$ (1st Tds)
- $s = s(P, T) \rightarrow ds = \left(\frac{\partial s}{\partial T}\right)_P dT + \left(\frac{\partial s}{\partial P}\right)_T dP$
 $C_P = T \left(\frac{\partial s}{\partial T}\right)_P$ & $\left(\frac{\partial s}{\partial P}\right)_T = - \left(\frac{\partial v}{\partial T}\right)_P$, Maxwell's Relation (D)
 $Tds = C_P dT - T \left(\frac{\partial v}{\partial T}\right)_P dP$ (2nd Tds)
- $s = s(P, v) \rightarrow ds = \left(\frac{\partial s}{\partial P}\right)_v dP + \left(\frac{\partial s}{\partial v}\right)_P dv$
 $C_v = T \left(\frac{\partial s}{\partial T}\right)_v$ & $C_P = T \left(\frac{\partial s}{\partial T}\right)_P$
 $Tds = C_v \left(\frac{\partial T}{\partial P}\right)_v dP + C_P \left(\frac{\partial T}{\partial v}\right)_P dv$ (3rd Tds)



Internal Energy, u

- $u = u(v, T) \rightarrow du = \left(\frac{\partial u}{\partial T}\right)_v dT + \left(\frac{\partial u}{\partial v}\right)_T dv = C_v dT + \left(\frac{\partial u}{\partial v}\right)_T dv$
- $du = Tds - Pd v = C_v dT + T \left(\frac{\partial P}{\partial T}\right)_v dv - Pd v$ (\leftarrow 1st Tds Eq.)
 $\left(\frac{\partial u}{\partial v}\right)_T = T \left(\frac{\partial P}{\partial T}\right)_v - P$
 $du = c_v dT + [T \left(\frac{\partial P}{\partial T}\right)_v - P] dv$
- Ideal gas: $\left(\frac{\partial u}{\partial v}\right)_T = \left[\frac{RT}{v} - P\right] = 0$
 $\left(\frac{\partial u}{\partial v}\right)_T = 0 = \left(\frac{\partial u}{\partial P}\right)_T \left(\frac{\partial P}{\partial v}\right)_T = -\frac{P}{v} \left(\frac{\partial u}{\partial P}\right)_T \rightarrow \left(\frac{\partial u}{\partial P}\right)_T = 0$
 $\left(\frac{\partial u}{\partial v}\right)_T = 0 \rightarrow u \neq f(v): \left(\frac{\partial u}{\partial P}\right)_T = 0 \rightarrow u \neq f(P)$
 $\rightarrow du = C_v dT = f(T)$
- van der Waals' gas:
 $\left(\frac{\partial u}{\partial v}\right)_T = \frac{RT}{v-b} - P = \frac{a}{v^2} \rightarrow du = C_v dT + \frac{a}{v^2} dv = f(T, v)$



Enthalpy, h

- $h = h(P, T) \rightarrow dh = \left(\frac{\partial h}{\partial T}\right)_P dT + \left(\frac{\partial h}{\partial P}\right)_T dP = C_p dT + \left(\frac{\partial h}{\partial P}\right)_T dP$
- $dh = Tds + dP = C_p dT - T \left(\frac{\partial v}{\partial T}\right)_P dP + v dP$ ($\leftrightarrow 2^{nd} Tds$ Eqn.)

$$\left(\frac{\partial h}{\partial P}\right)_T = v - T \left(\frac{\partial v}{\partial T}\right)_P$$

$$dh = c_p dT + \left[v - T \left(\frac{\partial v}{\partial T}\right)_P\right] dP$$

- Ideal gas: $\left(\frac{\partial h}{\partial P}\right)_T = v - \frac{TR}{P} = 0 \rightarrow h \neq f(P)$
 $\left(\frac{\partial h}{\partial P}\right)_T = 0 = \left(\frac{\partial h}{\partial v}\right)_T \left(\frac{\partial v}{\partial P}\right)_T = -\frac{v}{P} \left(\frac{\partial h}{\partial v}\right)_T \rightarrow \left(\frac{\partial h}{\partial v}\right)_T = 0$
 $\left(\frac{\partial h}{\partial P}\right)_T = 0 \rightarrow h \neq f(P) : \left(\frac{\partial h}{\partial v}\right)_T = 0 \rightarrow h \neq f(v)$

$$\rightarrow dh = C_p dT = f(T)$$

- van der Waals' gas: $\Rightarrow h = f(T, P)$

 $C_p - C_v$

- $s = s(v, T) \rightarrow ds = \left(\frac{\partial s}{\partial T}\right)_v dT + \left(\frac{\partial s}{\partial v}\right)_T dv$
 $\left(\frac{\partial s}{\partial T}\right)_P = \left(\frac{\partial s}{\partial T}\right)_v + \left(\frac{\partial s}{\partial v}\right)_T \left(\frac{\partial v}{\partial T}\right)_P \leftrightarrow \left[\left(\frac{\partial s}{\partial T}\right)_P = \frac{C_p}{T}, \left(\frac{\partial s}{\partial v}\right)_T = \frac{C_v}{T}\right]$
 $\rightarrow C_p - C_v = T \left(\frac{\partial s}{\partial v}\right)_T \left(\frac{\partial v}{\partial T}\right)_P = T \left(\frac{\partial P}{\partial T}\right)_v \left(\frac{\partial v}{\partial T}\right)_P$

- $f(x, y, z) = 0 \rightarrow \left(\frac{\partial z}{\partial x}\right)_y \left(\frac{\partial y}{\partial z}\right)_x \left(\frac{\partial x}{\partial y}\right)_z = -1$
 $\rightarrow \left(\frac{\partial P}{\partial v}\right)_T \left(\frac{\partial T}{\partial P}\right)_v \left(\frac{\partial v}{\partial T}\right)_P = 1 \rightarrow \left(\frac{\partial P}{\partial v}\right)_T \left(\frac{\partial v}{\partial T}\right)_P = -\left(\frac{\partial P}{\partial T}\right)_v$

$$C_p - C_v = T \left(\frac{\partial P}{\partial T}\right)_v \left(\frac{\partial v}{\partial T}\right)_P = -T \left(\frac{\partial P}{\partial v}\right)_T \left(\frac{\partial v}{\partial T}\right)_P^2$$

- For liquids & solids, $\left(\frac{\partial v}{\partial T}\right)_P \rightarrow 0 \Rightarrow C_p \approx C_v \approx C$
- $\left(\frac{\partial v}{\partial T}\right)_P^2$ is +ve & $\left(\frac{\partial P}{\partial v}\right)_T$ is -ve for all known substances, $C_p \geq C_v$
- as $T \rightarrow 0$, $C_p \rightarrow C_v$, at $T = 0$, $C_p = C_v$



- Isothermal compressibility, $k_T \equiv -\frac{1}{v} \left(\frac{\partial v}{\partial P}\right)_T$
- Volume expansivity, $\beta \equiv \frac{1}{v} \left(\frac{\partial v}{\partial T}\right)_P$

$$C_p - C_v = -T \left(\frac{\partial P}{\partial v}\right)_T \left(\frac{\partial v}{\partial T}\right)_P^2 = \frac{\beta^2}{k_T} v T$$

- Ideal gas: $Pv = RT \rightarrow k_T = \frac{1}{P}$, $\beta = \frac{1}{T}$

$$C_p - C_v = R$$



Clausius-Clapeyron Equation (for Phase Change)

- $\left(\frac{\partial P}{\partial T}\right)_v = \left(\frac{\partial s}{\partial v}\right)_T = \frac{s_2 - s_1}{v_2 - v_1}$: phase change $\rightarrow T = T_{sat} = \text{const.}$
- $\left(\frac{\partial P}{\partial T}\right)_v = \frac{dP}{dT}$, for mixture of 2 phases, $P = f(T)$
- $\frac{dP}{dT} = \frac{s_2 - s_1}{v_2 - v_1} = \frac{h_2 - h_1}{T(v_2 - v_1)} \Rightarrow \left(\frac{dP}{dT}\right)_{sat} = \frac{h_{12}}{T v_{12}}$ Clapeyron Eqn.

Example: using only P-v-T data, estimate h_{fg} of R-134a at 20°C

- $v_{fg} = (v_g - v_f)_{sat, @20^\circ\text{C}} = 0.035153 \text{ m}^3/\text{kg}$
- $\left(\frac{dP}{dT}\right)_{sat, @20^\circ\text{C}} = \frac{\Delta P}{\Delta T}_{sat, @20^\circ\text{C}} = \frac{P_{sat, @24^\circ\text{C}} - P_{sat, @16^\circ\text{C}}}{24^\circ\text{C} - 16^\circ\text{C}} = 17.70 \text{ kPa/K}$
- $h_{fg} = T v_{fg} \left(\frac{dP}{dT}\right)_{sat, @20^\circ\text{C}} = (293.15)(0.035153)(17.70) = 182.40 \text{ kJ/kg}$
 Tabulated value of h_{fg} @ 20°C is 182.27 kJ/kg .

- $v_2 \gg v_1 \rightarrow v_2 = \frac{RT}{P} \Rightarrow \left(\frac{d \ln P}{d(1/T)}\right)_{sat} = -\frac{h_{fg}}{R}$ Clausius-Clapeyron Eq.

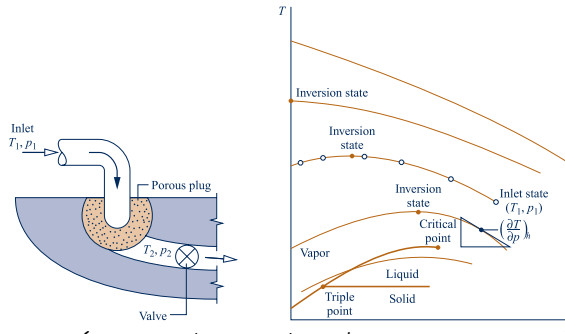
$$\rightarrow \ln \left(\frac{P_2}{P_1}\right)_{sat} = \frac{\Delta h}{R} \left(\frac{1}{T_1} - \frac{1}{T_2}\right)$$

- $\ln P_{sat} = A + \frac{B}{T} + C \ln T + DT$, widely used vapour-pressure Eq.



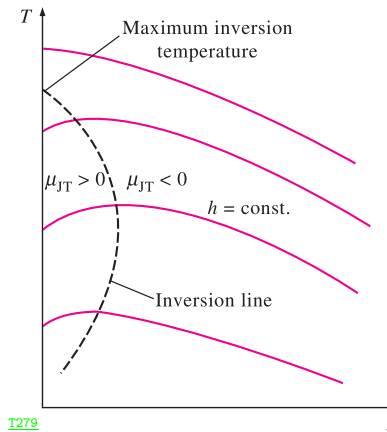
Gas Expansion & Joule-Thomson coefficient

The temperature behaviour of a fluid during a throttling process is described by Joule-Thomson coefficient, μ_{JT} .

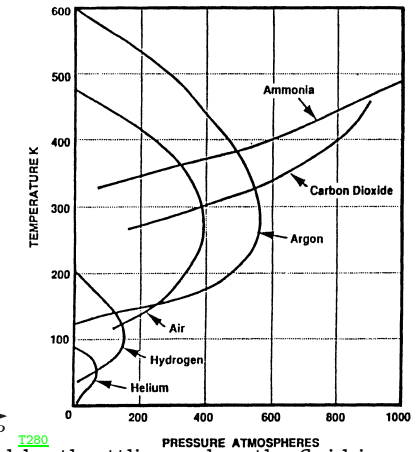


T278

$$\mu_{JT} \equiv \left(\frac{\partial T}{\partial P} \right)_h = \begin{cases} -ve & : \text{temperature increase} \\ 0 & : \text{temperature same} \\ +ve & : \text{temperature drop} \end{cases}$$



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T280

A cooling effect cannot be achieved by throttling unless the fluid is below its **maximum inversion temperature**. For hydrogen its value is -68°C and hydrogen must be cooled below this temperature if further cooling is to be achieved.

